

REMARKS

Claims 1-5 are active in the present application. The claims have been amended to remove multiple dependencies and for clarity. No new matter is added. An action on the merits and allowance of claims is solicited.

Respectfully submitted,

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IN THE SPECIFICATION

Please replace the title on page 1, with the following:

[OLD TITLE] NEW TITLE

IN THE CLAIMS

Please amend the claims as follows:

--1. (Amended) Process for producing cyanuric chloride, comprising trimerisation of cyanogen chloride in the presence of a washed activated carbon having a BET surface area of at least 1000 m<sup>2</sup>/g and an Fe content of less than 0.15 wt.%, [(]calculated as Fe<sub>2</sub>O<sub>3</sub>[)] at a temperature of at least 250 °C,

[characterised in that] wherein an activated carbon having an effective pore volume V<sub>eff</sub> of equal to or greater than 0.17 ml/g is used, V<sub>eff</sub> [being] is obtained from pores having a pore diameter in the range of 0.5 to 7 nm.

2. (Amended) Process according to claim 1,

[characterised in that an activated carbon is used, whose] wherein the effective pore volume V<sub>eff</sub> of the activated carbon is [formed] calculated from the sum [V<sub>eff</sub> = 0.25 . V<sub>micro</sub> +

0.5 V<sub>meso</sub>]  $V_{\text{eff}} = 0.25V_{\text{micro}} + 0.5V_{\text{meso}}$ , V<sub>micro</sub> [comprising] ~~represents~~ pores having a diameter of less than 2 nm and V<sub>meso</sub> [comprising] ~~represents~~ pores having a diameter of 2 to 30 nm.

3. (Amended) Process according to claim 1 [or 2, characterised in that] wherein

V<sub>eff</sub> of the activated carbon used is at least 0.2 ml/g.

4. (Amended) Process according to [one of claims 1 to 3, characterised in that] claim

1, wherein

the activated carbon [to be used] has a bulk density of equal to or less than 420 g/l.

5. (Amended) Process according to [one of claims 1 to 4, characterised in that] claim

1, wherein

the activated carbon [to be used] has a BET surface area of at least 1200 m<sup>2</sup>/g and V<sub>eff</sub> is at least 0.2 ml/g.--

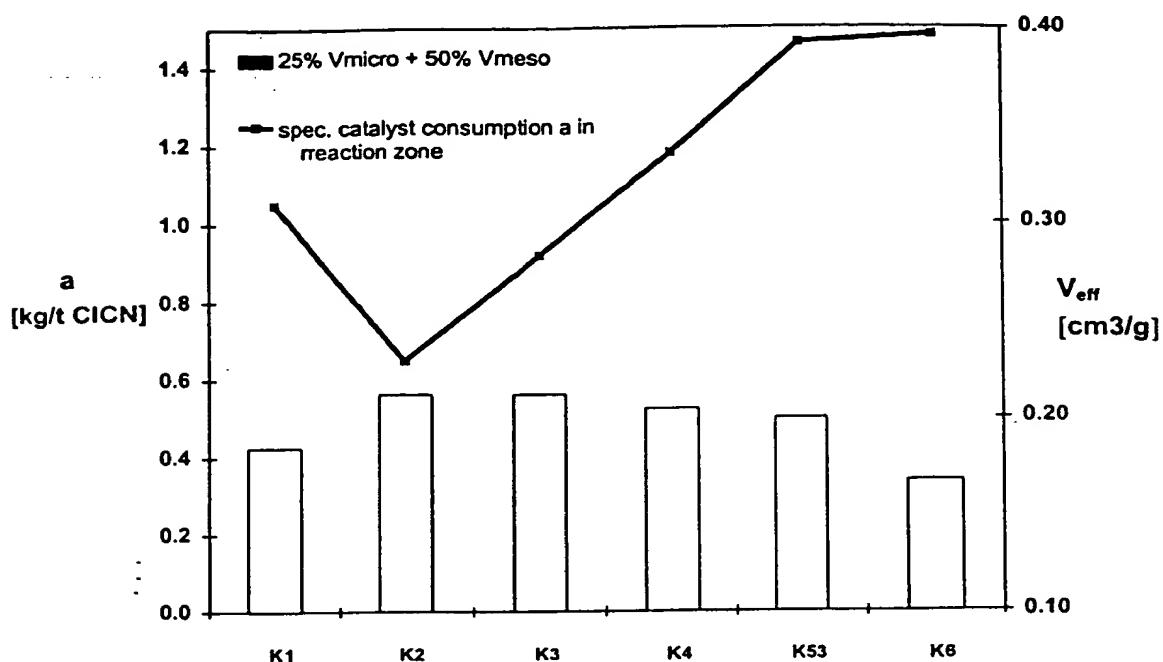


Fig. 1: Specific catalyst consumption a in relation to the effective pore volume

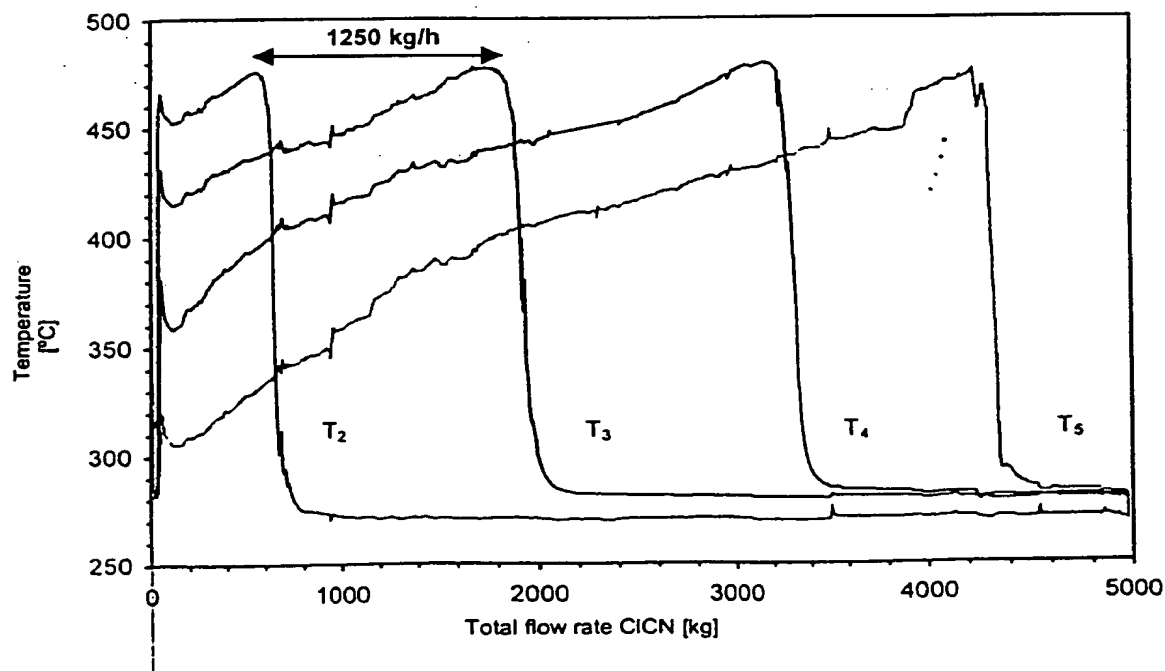


Fig. 2: Movement of the hot spot through the reactor